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㉓ Preparation of aminopropyltrialkoxysilanes and/or aminoalkylalkoxysilanes.

㉔ A platinum catalyzed addition of allylamine and N-substituted allyl amines to trialkoxysilanes or alkylalkoxysilanes is improved by running the reaction under pressure at 110-210°C and in the presence of a reaction promoter. As a result, the time and the amount of platinum catalyst required for the reaction are significantly reduced and conversion and yield of the product increased.

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PREPARATION OF AMINOPROPYLTRIALKOXYSILANES  
AND/OR AMINOALKYLALKOXYSILANES

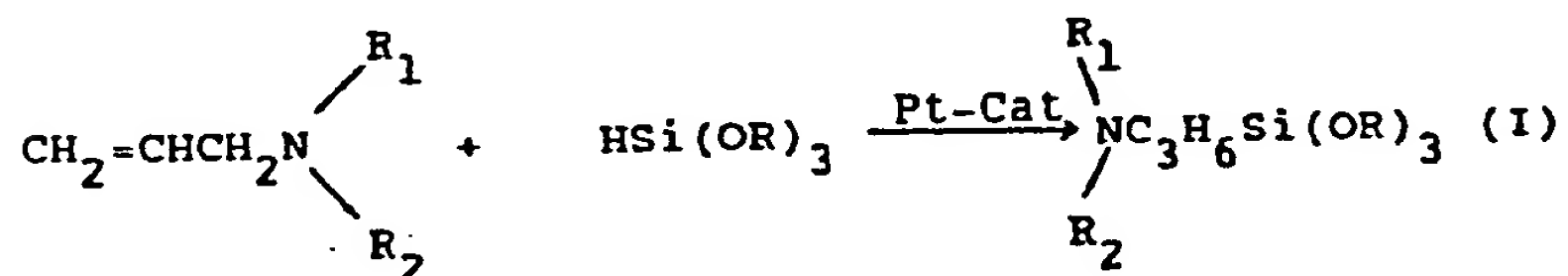
BACKGROUND OF THE INVENTION

FIELD OF THE INVENTION

The instant invention relates to a novel process for preparing aminopropyltrialkoxysilanes and/or aminoalkylalkoxysilanes. More specifically, the invention relates to the platinum catalyzed addition of allylamine or N-substituted allylamines with trialkoxysilanes or alkylalkoxysilanes under pressure at 110° to 210°C in the presence of a reaction promoter.

THE PRIOR ART

The platinum catalyzed addition of allylamine or N-substituted allylamines to trialkoxysilanes (I) offers a direct route to aminopropyltrialkoxysilanes. This reaction is well



known and has been studied by many investigators. However, in order to obtain a reasonable conversion and yield, the process requires long reaction time and/or high platinum catalyst concentrations. For instance, U.S. Patent No. 3,665,017 teaches the preparation of  $\gamma$ -aminopropyltriethoxysilane and  $\gamma$ -aminopropylalkylalkoxysilanes by refluxing allylamine with hydrogenalkoxysilanes or hydrogenalkylalkoxysilanes in the presence of a platinum catalyst

until the temperature of the reaction mixture reaches a constant level above 110°C. The time required to reach the final temperature varied from 10 to 60 hours, depending upon the platinum catalyst concentration used and the presence or absence of a solvent having a higher boiling point than the components that were to be added to one another. Therefore, when a mixture of allyl amine and triethoxysilane containing 5% of ethyl silicate was heated in the presence of approximately 200 ppm platinum (as  $H_2PtCl_6$ ), the temperature of the reaction rose to 190°C in 14 hours to give a 71-79% yield of the desired product. But the time required increased to more than two days (56 hours) when the platinum catalyst concentration was decreased to about 66 ppm. Similarly, in U.S. Patent No. 3,864,373 mixtures of  $\gamma$ - and  $\beta$ -amino-propyl-triethoxysilane were prepared by heating allyl amine with trialkoxysilane in the presence of a platinum catalyst such as mesityl oxide platinum dichloride until the sump temperature reached approximately 135°C or for 24 hours (Zh., Obshch Khim, 42, (4), 858-862 (1972)). In the latter case, the temperature of the reaction mixture rose from 74°C to 125°C during the 24 hour heating period and the yield of aminopropyltriethoxysilane was in the range of 60 to 67%. Two Czech Patents obtained 57-71% of  $\gamma$ -aminopropyltriethoxysilane by heating the reactants from 70-150°C in the presence of  $(CH_2=CHCH_2NH_3)^+PtCl_3^-$  (Czech C S 165,746) or of  $(Ph_3P)_4Pt$  or  $(Ph_3P)_2PtX_2$  (193,448).

Recently, a continuous process for the preparation of aminoalkoxysilanes was disclosed (Ger. (East) DDR151944). Thus the addition of organohydrosilanes to allyl amine in the presence of a solution or suspension of an addition catalyst in multi-stage, heatable reaction apparatus was carried out under ambient pressure in the temperature range of 110-135°C and with a contact time of from 3600-2400 seconds. According to the process, the reaction time was shortened considerably. However, the process requires several reactors and high platinum concentration (>200 ppm).

Aminopropyltriethoxysilanes have also been prepared by heating the reactants in the presence of a platinum catalyst and a promotor (or co-catalyst) such as unsaturated ether (USSR 372,228), ketone, carboxylic acids, keto-acids and esters (USSR 415,268) allyl alcohol (USSR 505647), epichlorohydrin (USSR 724,459) and dicarbon-nido-undecaborate  $K(C_2B_9H_{12-n}R^-K^+)$  (USSR 724,515). These reactions generally were carried out at atmospheric pressure and the platinum catalyst and promoter were heated together with allyl amine and the corresponding trialkoxysilane until the temperature of the reaction mixture reached 120°C or higher. For example, aminopropyl-trialkoxysilanes were prepared by treating trialkoxysilanes with allyl amine in the presence of  $H_2PtCl_6$  (100 ppm) and 0.1-1.5% epichlorohydrin for 9-11 hours until the temperature of the mixture reached 120°C and then held at that temperature for another 2-3 hours. Yield of the aminosilanes was in

the range of 58-70%. V. Vybrial and his coworkers have also studied the effect of various promoters which included: triphenylphosphine, triphenylarsine, carboxylic acids and their esters and some carbonyl compounds. The best modifier found was triphenylphosphine. When used in conjunction with  $H_2PtCl_6$  (~350 ppm Pt), it shortened the reaction time from 9.7 hours ( $H_2PtCl_6$  alone) to 6.5-7.3 hours. All these results indicate that even with 100-200 ppm of Pt, extensive reaction time is required in order to obtain reasonable conversions and yields.

#### OBJECT OF THE INVENTION

It is a primary object of the invention to provide a process for preparing aminotrialkoxysilanes and aminoalkylalkoxysilanes with a significantly reduced amount of platinum catalyst.

Another object of the invention is to obtain increased yields of aminotrialkoxysilanes and aminoalkylalkoxysilanes.

A third object of the invention is to shorten the reaction time necessary to provide acceptable yields of aminotrialkoxysilanes and aminoalkylalkoxysilanes.

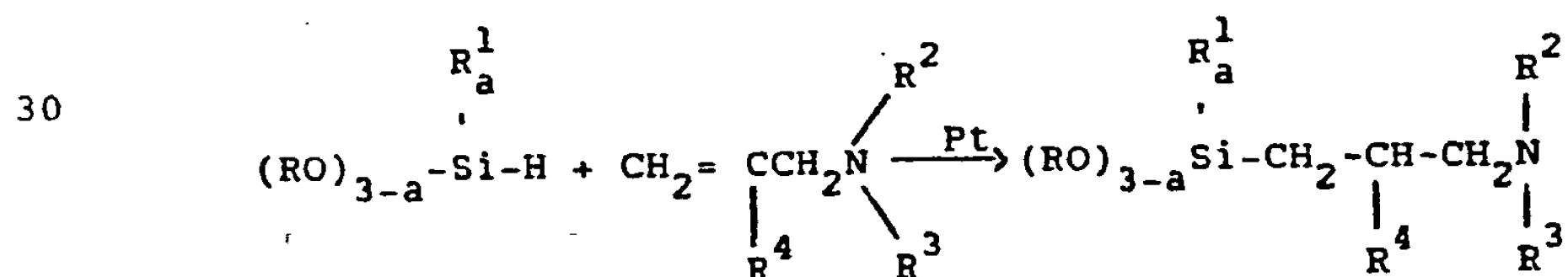
#### SUMMARY OF THE INVENTION

The present invention provides an improved process for preparing beta- and gamma- aminotrialkoxysilanes and aminoalkylalkoxysilanes. It has

been found that by running the addition reaction  
 between allylamine and/or N-substituted allylamine  
 with trialkoxy- silanes and/or alkylalkoxysilanes  
 under pressure, at high initial temperatures, in the  
 5 presence of a reaction promoter, the efficiency of  
 the platinum catalyst is greatly increased. As a  
 result of this improved process, the platinum  
 catalyst concentration necessary to obtain an  
 acceptable yield can be greatly reduced, while at  
 10 the same time significantly shortening the reaction  
 time. Furthermore, the yield of  
 aminopropyltrialkoxysilanes and/or  
 aminoalkylalkoxysilanes obtained is improved, as is  
 the conversion percentage. The high conversion and  
 15 yields achieved by such reduced amounts of platinum  
 catalyst have previously never been observed.  
 Indeed, U.S. Patent No. 3,665,027 stated that  
 reduced yields and conversion of amino-  
 propyltrialkoxysilanes would be expected when the  
 20 addition reaction is carried out under pressure and  
 at higher temperatures than reflux.

#### DETAILED DESCRIPTION OF THE INVENTION

In accordance with the present invention  
 25 there is provided a process for preparing  
 aminopropyltrialkoxysilanes and aminoalkylalkoxy-  
 silanes. The reaction is generally represented by  
 the sequence:

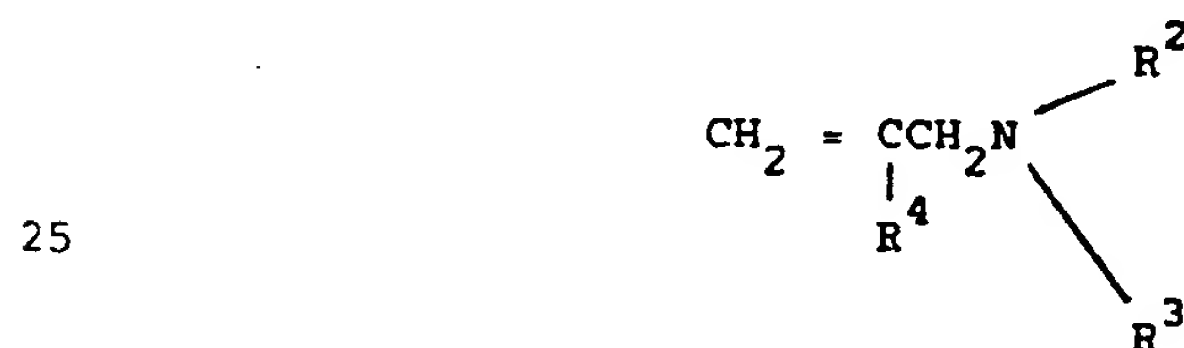


Suitable silanes are those selected from the group represented by the general formula:



wherein  $a$  is 0, 1 or 2, and  $R$  and  $R^1$  are individually monovalent hydrocarbon radicals containing from 1 to 10 carbon atoms. Preferably,  $a$  is 0 or 1 and  $R$  and  $R^1$  are methyl or ethyl groups. Illustrative of suitable silanes are triethoxysilane, trimethoxysilane, tripropoxysilane, tri-isopropoxysilane, tributoxysilane, methyldi-methoxysilane, ethyldimethoxysilane, methyldiethoxy-silane, dimethylmethoxysilane, trioctyloxysilane, methyldioctyloxysilane, and dimethyloctyloxysilane.

Suitable amines useful in the present invention are those selected from the group represented by the formula:



wherein  $R^2$  and  $R^3$  are independently selected from hydrogen, monovalent hydrocarbon groups containing from 1 to 10 carbon atoms, phenyl or substituted phenyl groups,  $-CH_2 \underset{\underset{R^4}{|}}{C} = CH_2$ , and  $-(CH_2 CH_2 NH)_n H$  wherein  $n$  is 1 to 4 and

$R^4$  is individually either hydrogen or a methyl

- 7 -

group. Preferably the amine is alkylamine where  $R^2$  and  $R^3$  are both hydrogen. Illustrative of suitable amines are allylamine, N,N-dimethylallylamine, N,N-diethylallylamine, N-allylaniline, methallylamine, diallylamine, triallylamine, <sup>and</sup> 4-

The ratio of silane to amine can be varied from 1.5:1 to 1:1.5, and preferably is within the range of 1.1:1 to 1:1.1 when allylamine and its derivatives are employed. The ratio of silane to amine will change to 2.0:1 to 2.5:1 when diallylamine and its derivatives are employed and 3.0:1 to 4.5:1 when triallylamine and its derivatives are used.

The reaction temperature and resultant pressure play an important role in the improved process. Suitable reaction temperatures range from 110° to 210°C and preferably in the range of from 130° to 170°C. The pressure will be a function of the boiling point of the reactants. Generally, the reaction will take place in a closed system to avoid volatilization of one or more of the reactants when its boiling point is below the operating temperatures, this in turn will result in increased operating pressures as the system approaches its operating temperature.

The reaction time will depend upon other conditions, such as the amount of platinum catalyst or the temperature of reaction. As would be expected, the higher the catalyst concentration and reaction temperature, the shorter the reaction time. Generally, when the platinum catalyst

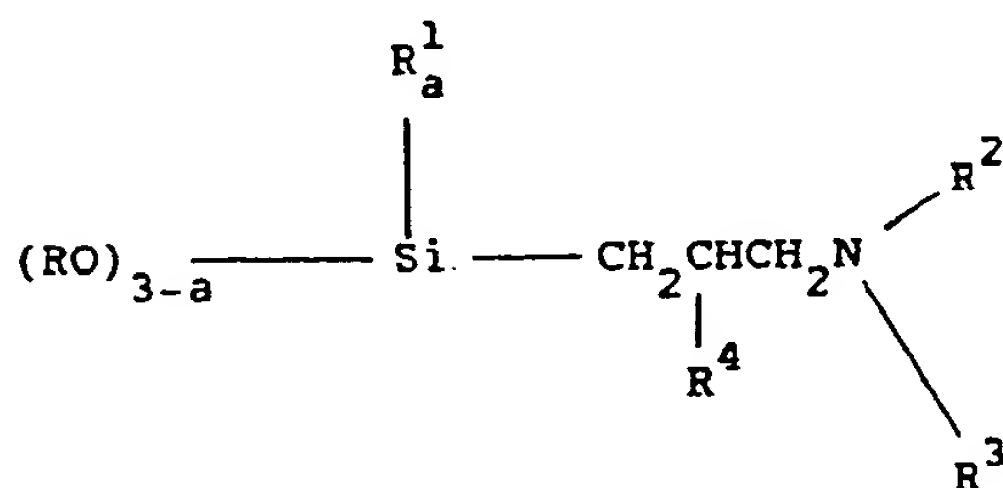


concentration is in the range of 10-20 parts per million, the reaction temperature is within the range of 130° to 170°C. A reaction time on the order of 2 to 5 hours is sufficient to obtain acceptable yields. Longer reaction times will not significantly increase the yield, but they may be desirable in certain instances. The platinum-containing hydrosilation catalyst may be chosen from the group of supported platinum catalysts such as platinum on  $\gamma$ -alumina or on charcoal, or from the group of soluble platinum complexes, such as chloroplatinic acid, bis(ethylene platinumous) chloride, cis-dichlorodiamine platinum (II), platinum (II) acetylacetonate, platinum (0) or other soluble platinum complexes well known in the art. The soluble platinum complexes are normally used as solutions in solvents such as isopropanol or 1,2-dimethoxyethane. The concentration of the platinum-catalyst required depends on reaction temperature and time but is generally used in the range of 5-30 ppm and preferably 10-25 ppm based on the total weight of the silane and amine used. Higher catalyst concentrations are not necessary nor economical.

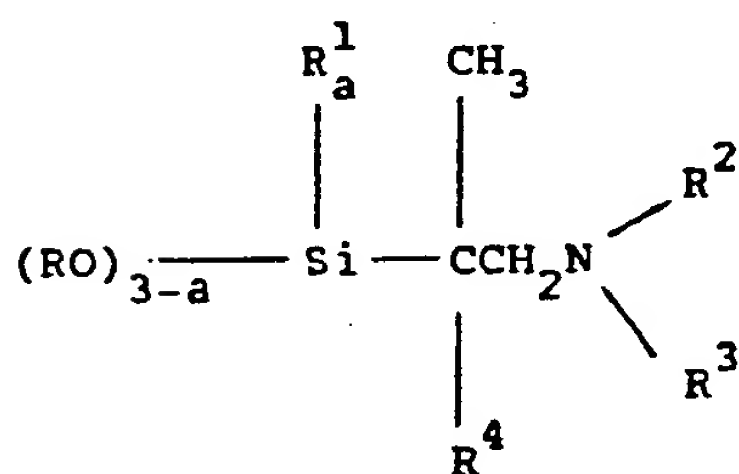
The use of a reaction promoter is preferable but not absolutely necessary. However, the presence of a reaction promoter is needed to further accelerate the rate of the reaction and increase the conversion of the reaction. The reaction promoter should be employed at a concentration of 0.5 to 10 mole percent of the silane charge, and preferably 1.5 to 2.5 mole

percent of the silane charged. Suitable reaction promoters include, but are not limited to, the alkali-metal carbonates or bi-carbonates, such as potassium carbonate, potassium bicarbonate, sodium carbonate, sodium bicarbonate, cesium carbonate, cesium bicarbonate, rubidium carbonate, rubidium bicarbonate, lithium carbonate, lithium bicarbonate, barium carbonate, barium bicarbonate, strontium carbonate, strontium bicarbonate, calcium carbonate and calcium bicarbonate.

The resulting aminopropyltrialkoxysilane and aminoalkylalkoxysilane obtained are mixtures of beta- and gamma- isomers and are generally represented by the formulae:



gamma-isomer

beta-isomer (when R<sup>4</sup> is hydrogen)

wherein R, R<sup>1</sup>, R<sup>2</sup>, R<sup>3</sup>, R<sup>4</sup> and a are as previously defined. The resulting amino propyltrialkoxysilane and aminoalkylalkoxysilane are

generally recovered in high yields and conversions when the catalyst concentration and temperature of the invention are employed as is demonstrated in the examples.

5 Illustrative of such products include the beta- and gamma- isomers of aminopropyltri-methoxysilane, aminopropyltriethoxysilane, aminopropylmethyldimethoxysilane, aminopropyl-  
10 tri-isopropoxysilane, N-phenylaminopropyltri-ethoxysilane, N-phenylaminopropylmethyldiethoxy-silane, tris-(triethoxysilylpropyl)amine, bis-(triethoxysilylpropyl)amine, tris-(trimethoxy-silylpropyl)amine, bis-(trimethoxysilylpropyl)amine, and  
15 N-(beta-aminoethyl)aminopropyltriethoxysilane,

Aminopropyltrialkoxysilanes and aminoalkylalkoxysilanes find general utility as potential glass-plastic coupling agents, bonding  
20 aids, additives to phenolic binder/foundry mixtures, adhesion promoters for vinyl plastisols, polyurethane elastomers, and epoxy and acrylic-based inks.

Whereas the exact scope of the instant invention is set forth in the appended claims, the  
25 following specific examples illustrate certain aspects of the present invention and, more particularly, point out methods of evaluating the same. However, the examples are set forth for illustration only and are not to be construed as  
30 limitations on the present invention except as set forth in the appended claims. All parts and percentages are by weight unless otherwise specified.

Example 1

5 Into a  $N_2$  purged 45 ml Parr bomb equipped with a pressure gauge, were added 0.07 grams of anhydrous  $Na_2CO_3$ , 9.2 ml of triethoxysilane, 3.8 ml of allyl amine and 15 ppm of Pt (as  $H_2PtCl_6$ ) under  $N_2$ . The bomb was placed in a fluidized sand bath which was pre-heated to  $130^\circ C$  and left there for 6.5 hours. At the end of the reaction, the bomb was taken out and cooled with ice-water. The  
10 content of the reaction mixture was analyzed with a Hewlett-Packard 5830-A gas chromatograph (G.C.).

The gas chromatograph was equipped with a 3 m (10 ft.) column packed with 10% UC-W98 on Chromasorb 750 (80/100 mesh). The GC conditions used were: He  
15 29-32 ml/min., Inj. Port  $300^\circ C$ , detector  $350^\circ C$ , program  $90^\circ C$  for four min. then  $90^\circ$ - $250^\circ C$  at a rate of  $20^\circ/min$ .

The conversion and yield of aminopropyltriethoxysilane were determined according to the  
20 internal standard method well known in the art. It was found that the conversion and yield of the reaction based on the triethoxysilane used were 71.3% and 86.6% respectively. The ratio of gamma to beta isomers was 3.9:1.  
25

Example 2

The same procedure of Example 1 was used except that 0.1 gram of  $Na_2CO_3$  was used and that the reaction temperature used was  $140^\circ C$ . Conversion  
30 and yield of the reaction were 79.1% and 81.4% respectively. The ratio of gamma to beta isomers was 4.7:1.

- 12 -

Example 3

5 The sample procedure of Example 1 was used except that  $\text{Na}_2\text{CO}_3$ , 0.10 gram, was used and that the reaction was carried out at  $130^\circ\text{C}$  for 12 hours. Conversion and yield of aminopropyltriethoxysilane were 80.5% and 83.4% respectively. The ratio of gamma to beta isomers was 4.2:1.

Example 4

10 The sample procedure of Example 3 was used except that no anhydrous  $\text{Na}_2\text{CO}_3$  was used. Percent conversion and yield of the reaction were 60.5% and 85.6% respectively. The ratio of gamma to beta isomers was 4.4:1.

Example 5

15 In order to find the actual time required under the conditions used, Swagelok capped stainless steel tubes (3 ml capacity) were used as reactors. For each run, a batch of reaction mixture (i.e., 9.2 ml  $(\text{EtO})_3\text{SiH}$ , 3.8 ml allyl amine and 15 ppm of Pt (as  $\text{H}_2\text{PtCl}_6$ ) was made and transferred (each 1.2 ml) to the tubes which contained the desired amount of anhydrous  $\text{Na}_2\text{CO}_3$  (0.0092g). The small  
20 reactors were placed in a rocker and heated with a fluidized sand bath preheated to  $130^\circ\text{C}$ . At desired time intervals, the tubes were taken out, cooled with ice-water and analyzed. The formation of aminopropyltriethoxysilane was completed within 3.5  
25 hours.  
30

Example 6

The same procedure of Example 5 was used except that no  $\text{Na}_2\text{CO}_3$  was used. The results

- 13 -

obtained demonstrate again that the hydrosilation took place quite well at 15 ppm of Pt level even without  $\text{Na}_2\text{CO}_3$  but after 3.5 hours the reaction was only 82.5% as complete as that of Example 5, and even after 6 hours the results of Example 5 were not obtained.

#### Example 7

The same procedure of Example 5 was used except that the temperature used was  $150^\circ\text{C}$ . The time required for this reaction to achieve the results of Example 5 was about 2 hours.

#### Example 8

The same procedure of Example 5 was used except that 10 ppm of Pt (as Pt (II) acetyl acetate) was used. The hydrosilation went well even with such low amount of Pt-level, achieving results similar to those reported in Example 6 in 1.1 hours.

#### Example 9

Into a 50 ml 3-necked round bottom flask, fitted with a condenser, a thermometer, and  $\text{N}_2$  inlet tubing, were added 9.6 ml of triethoxysilane, 4.2 ml of allyl amine and 100 ppm of Pt (as  $\text{H}_2\text{PtCl}_6$ ). The reaction mixture was heated at refluxing temperature for 24 hours until the temperature of the reaction mixture reach  $108^\circ\text{C}$ . GC analysis of the reaction mixture showed that percent conversion and yield of the reaction were 33.6 and 67.4% respectively. The gamma to beta isomer ratio was 8.3:1.

Comparison of the result obtained from this experiment with those obtained from examples 1-8 indicates clearly the effect of temperature.

### Example 10

The same procedure of Example 9 was used except that 0.22 gm of anhydrous  $\text{Na}_2\text{CO}_3$  was used together with the 100 ppm of Pt. The temperature of the reaction reached 101°C in 4.5 hours. Percent conversion and yield of aminopropyltriethoxysilane were 55.4 and 71.2% respectively. The gamma to beta isomer ratio was 14.6:1.

### Example 11

The same procedure of Example 9 was used except that 50 ppm of Pt (as  $\text{H}_2\text{PtCl}_6$ ) was used instead of 100 ppm of Pt, and that 1.0 grams of  $\text{Na}_2\text{CO}_3$  was used. The reaction temperature reached  $100^\circ\text{C}$  after 7.3 hours. Percent conversion and yield of reaction were 41.2 and 67.5% respectively. The gamma to beta isomer ratio was 15.9:1.

The results from these examples indicate that addition of  $\text{Na}_2\text{CO}_3$  as a promoter shortens the reaction time and improves the conversion of the reaction.

### Example 12

The procedure given in Example 3 was followed except that methyldiethoxysilane (9.6 ml) was used instead of triethoxysilane and that 4.5 ml of allyl amine was used. Percent conversion and yield of the reaction were 71.5 and 85.7%.

- 15 -

respectively. The gamma to beta isomer ratio was 8.0:1.

#### Example 13

5           The same procedure given in Example 1 was followed except that the reactants used were: 0.20 gram of anhydrous  $\text{Na}_2\text{CO}_3$ , 9.6 ml of tri-isopropoxysilane, 3.8 ml of allyl amine and 20 ppm of Pt (as  $\text{H}_2\text{PtCl}_6$ ). The reaction was heated at  $140^\circ\text{C}$  to give a mixture of beta and gamma aminopropyltriisopropoxysilane isomers. Conversion and yield of reaction were 56.3% and 79.6% respectively.

#### Example 14

15           The procedure of Example 1 was followed except that the reactants were:  $\text{Na}_2\text{CO}_3$  0.15 gram, triethoxysilane 9.2 ml, N-allylaniline 6.8 ml and 11.4 ppm of Pt (as  $\text{H}_2\text{PtCl}_6$ ). The reaction mixture was heated at  $130^\circ\text{C}$  for 7 hours.

20           The reaction product was analyzed with a 10 ft. column packed with 10% OV-101 on chromasorb W-HP. Program used was:  $100^\circ\text{C}$  for one minute,  $100-325^\circ\text{C}$  at  $15^\circ/\text{min}$ . The major component of the reaction product was found to be a mixture of beta and gamma isomers of N-phenylaminopropyltriethoxysilane, which had 78.15% area % of the gas chromatogram.

#### Example 15

30           The same Swagelok capped stainless tubes of Example 5 were used. A batch reaction mixture was made by mixing 9.2 ml of triethoxysilane with 3.8 ml of allyl amine. The mixture, 2.6 ml each, was then



5 charged to the stainless tubes, each containing 0.0199 grams of anhydrous  $\text{Na}_2\text{CO}_3$  and a desired amount of one of the Pt-catalysts listed in Table 1. The tubes were heated at  $130^\circ\text{C}$  in a fluidized sand bath for 5 hours. Results obtained are summarized in Table 1.

TABLE 1

HYDROSILATION OF ALLYL AMINE WITH TRIETHOXY-SILANE

No.	Pt-catalyst	Wt of	Conv.	Yield	gamma/ beta isomer ratio
		Pt-cat. (g)			
1	$\text{PtCl}_2(\text{Ph}_3\text{P})_2$	0.0002	66.7	76.1	5.9
2	$\text{cis-Pt}(\text{NH}_3)_2\text{Cl}_2$	0.001	70.7	79.3	5.1
3	$(\text{Ph}_3\text{P})_4\text{Pt}$	0.004	66.2	74.7	5.9

Example 16

20 The same procedure of Example 1 was used except that 0.1 gram of anhydrous  $\text{Na}_2\text{CO}_3$  and 17 ppm of Pt were used and that the reaction was carried out at  $200^\circ\text{C}$  for 5 hours. Conversion and yield of the reaction were 56.2 and 58.7% respectively. The gamma to beta isomer ratio was 3.2:1.

Comparative Example A

30 The same procedure of Example 16 was used except that the reaction was carried out at  $230^\circ\text{C}$  for 5 hours. Conversion and yield of the reaction were 41.6 and 41.9% respectively. Therefore although the reaction will take place at reaction temperatures higher than  $210^\circ\text{C}$ , yield and conversion

of the desired product will drop because of other by-products formation. The gamma to beta isomer ratio was 2.8:1.

5

Comparative Example B

The same procedure of Example 1 was used except that 0.44 gram of  $\text{Na}_2\text{CO}_3$  and 66 ppm of Pt were used and that the reaction was carried out at 105-106°C for 5 hours. Yield and conversion of the reaction were 75.2 and 71.8% respectively. This result indicates that a higher amount of Pt-Catalyst is required when the reaction is carried out at reaction temperature lower than 110°C.

10

15

Example 17

Into a 50 ml 3-necked round bottom flask, fitted with a condenser, a thermometer, an addition funnel and  $\text{N}_2$  inlet-outlet tubing were added 0.44 g of anhydrous  $\text{Na}_2\text{CO}_3$ , 3.0 ml of diallylamine and 3.0 ml of triethoxysilane. The mixture was heated with an oil-bath at 120-125°C. Platinum catalyst (15 ppm as  $\text{H}_2\text{PtCl}_6$ ) was then added. Triethoxysilane was dropped in at such a rate that the temperature of the reaction mixture was maintained at 124-126°C. After the addition of  $(\text{EtO})_3\text{SiH}$  was completed, the mixture was heated at -120°C for 1.5 hours. Gas chromatographic analysis of the mixture indicated that the reaction gave a mixture of gamma- and beta- isomers of  $((\text{EtO})_3\text{SiC}_3\text{H}_6)_2\text{NH}$ . The total GC area % of the isomers was 85.04%.

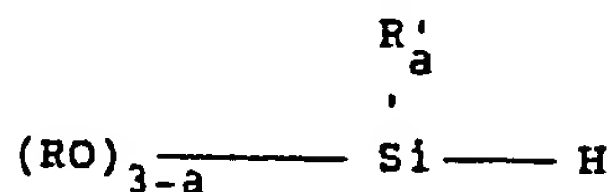
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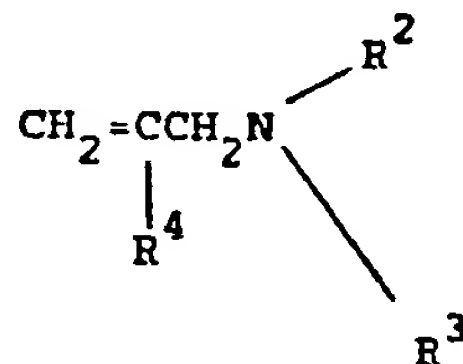
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Claims

1. A process for preparing aminoalkylalkoxysilanes which comprises reacting a hydrosilane of the general formula



wherein a is 0, 1 or 2, and R and R' are individually monovalent hydrocarbon radicals containing from 1 to 10 carbon atoms with an amine of the general formula



wherein R<sup>2</sup> and R<sup>3</sup> are individually selected from hydrogen, monovalent hydrocarbon radicals containing from 1 to 10 carbon atoms, a phenyl or substituted phenyl group -CH<sub>2</sub>C(=CH<sub>2</sub>)<sub>4</sub>, and -(CH<sub>2</sub>CH<sub>2</sub>NH)<sub>n</sub>H, wherein



n is 1 to 4 and R<sup>4</sup> is individually either hydrogen or a methyl group. Said reaction taking place under pressure at a temperature of from 110° to 210°C in the presence of a platinum-catalyst and, optionally, in the presence of a reaction promoter.

2. The process of claim 1 wherein the reaction temperature is from 130°C to 170°C.

3. The process of claims 1 or 2 wherein the platinum catalyst concentration is from 5 to 30 ppm, preferably from 10 to 25 ppm based on the total weight of the silane and amine charge.

5

4. The process of claims 1 to 3 wherein the reaction promoter is used at a concentration of 0,5 to 10 mole percent preferably from 1,5 to 2,5 mole percent of the silane charge.

10

5. The process of claims 1 to 4 wherein the silane is such that a is 0 or 1 and R and R<sup>1</sup> are either methyl or ethyl groups.

15

6. The process of claims 1 to 5 wherein the amine is such that R<sup>2</sup>, R<sup>3</sup> and R<sup>4</sup> are all hydrogen.

7. The process of claim 6 wherein the amine is methallylamine, diallylamine or triallylamine.

20

8. The process of claims 1 to 7 wherein the ratio of silane to amine as such is between 1.5:1 to 1:1.5 when the amine is alkylamine or its derivative, 2.0:1 to 2.5:1 when the amine is diallylamine or its derivative, and 3.0:1 to 4.5:1 when the amine is triallylamine or its derivative.

25

9. The process of claims 1 to 8 wherein the reaction promoter is an alkali-metal carbonate or bicarbonate.

30

10. The process of claim 9 wherein the reaction promoter is sodium carbonate or bicarbonate.